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## Technoeconomics and Sustainability of Renewable Methanol and Ammonia Productions Using Wind Power-based Hydrogen

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### Abstract

This study analyzes and compares the economics and sustainability aspects of two hydrogenation processes for producing renewable methanol and ammonia by using wind-power based electrolytic hydrogen. Carbon dioxide from an ethanol plant is used for producing methanol, while the nitrogen is supplied by an Air Separation Unit (ASU) for producing ammonia. The capacities are 99.96 mt/day methanol and 1202.55 mt/day anhydrous ammonia. The methanol plant requires 138.37 mt CO<sub>2</sub>/day and 19.08 mt H<sub>2</sub>/day. The ammonia is synthesized by using 217.72 mt H<sub>2</sub>/day and 1009.15 mt N<sub>2</sub>/day. The production costs and the carbon equivalent emissions (CO<sub>2</sub>e) associated with the methanol and ammonia processes, electrolytic hydrogen production, carbon capture and compression, and ASU are estimated. The integral facilities of both the methanol and ammonia productions are evaluated by introducing a multi-criteria decision matrix containing economics and sustainability metrics. Discounted cash flow diagrams are established to estimate the economic constraints, unit product costs, and unit costs of hydrogen. The hydrogen cost is the largest contributor to the economics of the plants. For the methanol, the values of emissions are -0.85 kg CO<sub>2</sub>e/kg methanol as a chemical feedstock and +0.53 kg CO<sub>2</sub>e/kg methanol as a fuel with complete combustion. For the ammonia, the value of emission is around 0.97 kg CO<sub>2</sub>e/kg ammonia. The electrolytic hydrogen from wind power helps reduce the emissions; however, the cost of hydrogen at the current level adversely affects the feasibility of the plants. A multi-criteria decision matrix shows that renewable methanol and ammonia with wind power-based hydrogen may be feasible compared with the nonrenewable ones and the renewable methanol may be more favorable than the ammonia.

**Keywords:** Electrolytic hydrogen production; Methanol production; Ammonia production; Technoeconomic analysis; Sustainability metrics; Multi-criteria decision matrix

### Introduction

Electrolytic hydrogen using wind power may serve as a feedstock for hydrogenation processes and hence chemical storage for renewable electricity [1-5]. Hydrogen is a clean fuel; its burning causes no harmful emissions; however the cost to produce, store, compress, and transport of the hydrogen is still high [6-12]. Methanol may be used as a fuel and a valuable feedstock for producing methyl t-butyl ether, dimethyl ether, dimethyl carbonate, formaldehyde, acetic acid and other chemical secondary intermediates which are used in producing plywood, particleboard, foams, resins and plastics [13-21].

Methanol production using fossil fuels, mainly from natural gas and coal, is a mature technology [13]. Renewable hydrogen-based methanol as an alternative fuel is widely investigated by researchers worldwide [1,2,13,22-24]. CO<sub>2</sub> may come from flue gas, gasification of biomass, or ethanol plants [1,13,25]. Energy analysis of recycling CO<sub>2</sub> and reaction mechanisms of hydrogenation of CO<sub>2</sub> are some of the efforts toward non-fossil fuel-based methanol as a renewable energy storage and carrier [26-32]. Rihko-Struckmann et al. [33] carried out an energetic evaluation in order to assess the overall efficiency of methanol and hydrogen-based storage systems for renewable electric energy; the efficiency of the system using hydrogen is higher compared with that of using methanol as the storage medium; however, storage and handling of methanol as chemical storage is favorable when compared with H<sub>2</sub> [18-20,33-36].

The utilization of CO<sub>2</sub> as carbon source for chemical synthesis could have a positive but only marginal impact on the global carbon balance [1,14]. Because, we add 3500 million mt CO<sub>2</sub>/year worldwide, while we use only 110 million mt CO<sub>2</sub>/year to produce other chemicals

(mainly urea); this is only around 3% usage of the CO<sub>2</sub> as feedstock [1,2,14,20,30]. On the other hand, the utilization of CO<sub>2</sub> in the fuel production or as a chemical storage of energy, such as methanol, could make a significantly larger impact, as only 16.8% of the world oil consumption was used in 2007 for non-energy purposes [14,17,36].

Like methanol, ammonia is a feedstock for manufacturing fertilizers such as urea, and may be considered as a chemical storage medium of renewable electricity [37-42]. Pure nitrogen for ammonia synthesis is produced using an air separation unit. In the U. S., about 98% of ammonia is produced by catalytic steam reforming of natural gas, while about 77% of world ammonia capacity is based on natural gas. The total energy consumption for the production of ammonia in a modern steam reforming plant is 40-50% above the thermodynamic minimum [40-42].

This study evaluates and compares the economics and sustainability aspects of the hydrogenation processes for renewable methanol and ammonia productions. A multi-criteria decision matrix is introduced in the feasibility evaluations of these productions. The cost and emissions for hydrogen, nitrogen, and CO<sub>2</sub> feeds used in these productions are estimated and the renewable hydrogen, methanol and ammonia economics are reassessed.

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## Sustainability in Chemical Processes and Energy Technology

The following sustainability metrics are applicable to specific chemical processes and energy systems [43-46]:

- Material intensity (nonrenewable resources of raw materials, solvents/unit mass of products)
- Energy intensity (nonrenewable energy/unit mass of products)
- Potential environmental impact (pollutants and emissions/unit mass of products)
- Potential chemical risk (toxic emissions/unit mass of products)

This study uses a comparative assessment of the renewable methanol and ammonia plants with the sustainability metrics of material intensity, 'energy intensity' and 'potential environmental impact' as emissions of CO<sub>2</sub>e by using the 'Carbon Tracking' and the 'Global Warming Potential' options of Aspen Plus [47]. The costs/unit mass of products are also considered in these metrics.

Table 1 shows the U.S. average Levelized Costs of Electricity (LCE) for generating technologies entering service in 2019 projected in the Annual Energy Outlook 2014 [2]. LCEs are estimated in 2012 \$/MWh and measures of the overall competitiveness of different generating technologies over an assumed financial life and duty cycle. The cost of Carbon Capture and Storage (CCS) accounts for 21% of the total LCE in Integrated Gasification of Combined Cycle (IGCC). For natural gas-based advanced combined cycle, the cost of CCS accounts for 29% of the total LCE. Wind-based electricity is becoming comparable with the hydropower, IGCC with CCS, and natural gas-based advanced combined cycle with CCS, although the cost of offshore-based wind power still remains high [2,12,48-50].

This study employs the CO<sub>2</sub>e emission factor data source of US-EPA-Rule-E9-5711 and the fuel source of natural gas [47,51,52]. Carbon equivalent emission, CO<sub>2</sub>e, indicates the global warming potential of GHGs; this study uses US-EPA with a predetermined cost for CO<sub>2</sub> fee/tax of \$/mt CO<sub>2</sub>e.

## Hydrogen Production

Currently, 96% of H<sub>2</sub> is produced directly from fossil fuels and about 4% is produced indirectly by using electricity generated through fossil fuels [53]. The conventional technologies are steam reforming of natural gas, coal gasification, and partial oxidation of hydrocarbons such as biomass. Renewable hydrogen comes from the electrolysis of water using hydropower, wind power, and solar photovoltaic power [54-56].

## Hydrogen Production from Syngas

Commercial processes for H<sub>2</sub> production are based on syngas feedstock produced from natural gas steam reforming (Figure 1) and coal (or biomass) gasification (Figure 2) with carbon capture and storage. These processes are complex, sensitive to the feedstock quality, and require large investments for larger units. The generated CO can also be used in the water-gas shift reaction to yield more hydrogen. In these processes, however, at least 20% of the energy of the fossil fuel is lost as waste heat.

Energy efficiency for biomass-based H<sub>2</sub> production is around 60% and likely become competitive in the future [55]. A representative

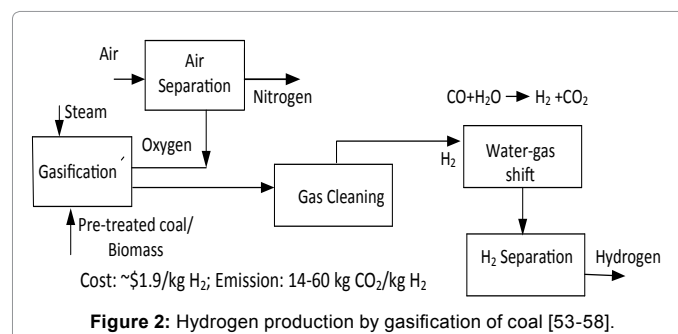
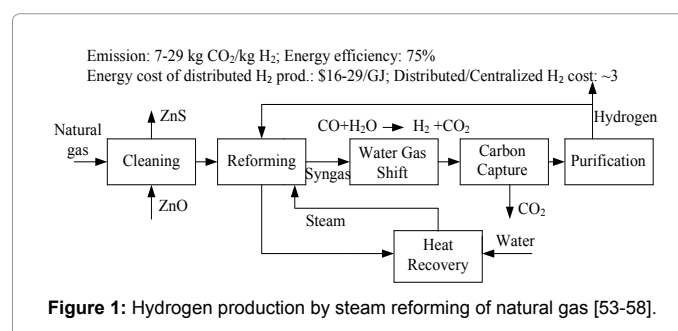
gasification reaction of biomass is  $C_aH_b + O_2 \rightarrow H_2 + CO + CO_2 + H_2O$ . Here the biomass reacts with oxygen supplied by an air separation unit (ASU) at 1150°C-1400°C and 400-1200 psig. Most modern plants purify the crude H<sub>2</sub> to 99.99-wt% by removing methane, CO<sub>2</sub>, N<sub>2</sub>, and CO using multi-bed pressure swing adsorption [53-59].

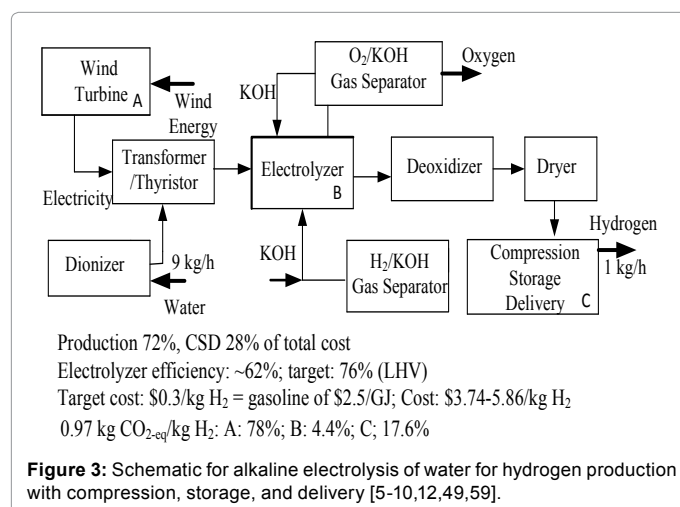
Current production of H<sub>2</sub> from natural gas and coal accounts for 48% and 18% of the total production, respectively. The emission of CO<sub>2</sub> varies between 7.33 kg CO<sub>2</sub>/kg H<sub>2</sub> and 29.33 kg CO<sub>2</sub>/kg H<sub>2</sub> using conventional fuels at about 75% energy efficiency. CO<sub>2</sub> emission (beside SO<sub>x</sub> and NO<sub>x</sub>) associated with producing H<sub>2</sub> from coal is about two-three times higher than that of the H<sub>2</sub> produced from natural gas [2,5-8,11,12].

## Hydrogen Production from Water Electrolysis

Renewable option is electro-chemical conversion by water electrolysis using electricity from renewable sources or nuclear power [49,50,53-58]. Figure 3 shows the schematic of wind power-based hydrogen production. Alkaline electrolysis technologies are the most mature commercial systems. The electrolyzer units use process water for electrolysis, and cooling water for cooling. KOH is needed for the electrolyte in the system. The system includes the following equipment: transformer, thyristor, electrolyzer unit, feed water demineralizer, hydrogen scrubber, gas holder, two compressor units to 30 bar, deoxidizer, twin tower dryer (Figure 3) [5,49]. These electrolyzers have the energy efficiencies (57%-75%) based on higher heating value- HHV and 50-60% based on the lower heating value-LHV. The typical current density is 100-300 mA/cm<sup>2</sup> [12,49].

The amount of total water used is 26.7 kg/kg H<sub>2</sub>; electrolysis uses approximately 45%, while manufacturing the wind turbines and the hydrogen storage consume around 38% and 17% of the total water used, respectively. The total greenhouse gas emission is 0.97 kg CO<sub>2</sub>e/kg H<sub>2</sub>, which is distributed as 0.757 kg CO<sub>2</sub>e/kg H<sub>2</sub> (78%) for the wind turbine production and operation (because of steel and concrete used in its construction), 0.043 kg CO<sub>2</sub>e/kg H<sub>2</sub> (4.4%) for the electrolyzer construction and operation, and 0.17 kg CO<sub>2</sub>e/kg H<sub>2</sub> (17.6%) for the





hydrogen compression and storage (mainly due to the production of steel used in the storage tanks) [59].

M-Langer et al. [54] evaluated hydrogen production processes based on natural gas steam reforming, coal and biomass gasification, and water electrolysis. H<sub>2</sub> production cost is around \$65/GJ using wind electricity, \$30/GJ using nuclear power, and \$600/GJ using photovoltaic electricity based on 2007 \$. Large-scale processes, using natural gas and coal, are the most economical processes while biomass gasification still needs technological improvements. The operating cost of an electrolyzer is driven by the energy efficiency and the cost of electricity. Energy efficiency needs to be increased to 76% from the current average of about 62%. The capital costs of wind-based H<sub>2</sub> are \$2086/kW (2011) and \$2067/kW (2012) for 50000 kg H<sub>2</sub>/day for a centralized production plant. New classes of materials could be designed at the nanoscale to produce catalysts that are more selective, less prone to poisoning, and able to operate at lower temperatures [5-9]. High-temperature solid oxide electrolysis can use lower cost energy (in the form of steam) for water-splitting to decrease electricity consumption [12,49].

## Economics of Wind Power-Based Hydrogen

Wind power-based electrolysis production cost estimates are limited geographically and the base cost of H<sub>2</sub> ranges from \$3.74/kg H<sub>2</sub> to \$5.86/kg H<sub>2</sub>. Capacities of H<sub>2</sub> productions range from 1,000 to 50,000 kg H<sub>2</sub>/day [2-5]. Other factors such as large-scale storage, compression, pipeline transport, and dispensing economics need separate analyses [49]. Currently, the production of H<sub>2</sub> by electrolysis using renewable electricity is not competitive with chemical production methods based on fossil fuels. However, using the off-peak power could increase plant load factor and improve the economics [49,53]. Electrolytic H<sub>2</sub> may be more attractive for regions without access to natural gas or if H<sub>2</sub> is used as an energy storage medium [33,49].

The current capital equipment cost for advanced electrolysis is between \$600/kW and \$700/kW. This cost needs to be reduced to \$200/kW to achieve \$2.75/GGE (untaxed gasoline gallon equivalent) by 2015 [49,50]. This shows around 60% of the improvement needed. Table 2 shows some electrolyzer types with their efficiencies. Higher efficiencies are possible with Polymer Electrolyte Membrane (PEM) and Solid Oxide Electrolytic Cell (SOEC) electrolyzers, which are still under development. Table 3 shows a typical sensitivity analysis to determine how the availability of wind farms and the capacity of electrolyzer affect the electricity needed for the production of H<sub>2</sub> [53-56]. Capital cost of

electrolyzer increases considerably as the wind farms' availability and electrolyzer capacity decrease.

Integration with low-cost renewables and the flexibility to produce H<sub>2</sub> from the grid electricity during off-peak periods may help lower the production cost of H<sub>2</sub>. A large alkaline (bipolar design) electrolyzer unit is the Norsk Hydro Atmospheric Type No. 5040, which can produce 1046 kg H<sub>2</sub>/day (381,790 kg H<sub>2</sub>/year) by using approximately 2.3 MW of electricity. Small systems however, are often built around Polymer Electrode Membrane (PEM) electrolyzer cell technology. Table 4 shows the streams of the Norsk hydro atmospheric type electrolyzer unit. The levelized cost is \$6.63/kg H<sub>2</sub> (2007\$) and the purchased electrolyzer system cost: \$489/kW (2014\$) [5-10]. Economic analysis shows that final production cost is around \$4.97/kg H<sub>2</sub>, which is much higher compared with the cost of \$1.91/kg H<sub>2</sub> from coal gasification [9,10].

The gas output streams from the electrolyzer are assumed to be 100% pure (typical real outputs are 99.9 to 99.9998% for H<sub>2</sub> and 99.2 to 99.9993% for O<sub>2</sub>). Electricity cost is typically 70 to 80% of the total cost of H<sub>2</sub> production. Table 5 shows the typical energy usage by the Norsk electrolyzer. The system energy requirement includes compression to bring the gas output to 33 bar (480 psi) [7,8]. The minimum power conversion system would require rectification of the variable ac output from the wind turbines to dc output for the electrolyzer cells. Future energy requirements are targeted at 50 kWh/kg H<sub>2</sub> [9,10,57-59].

Hydrogen production costs change approximately from \$1.75/kg H<sub>2</sub> to \$4.6/kg H<sub>2</sub> as the electricity prices change from \$0.02/kWh to \$0.08/kWh, for an advanced electrolyzer technology at 76% efficiency, and capital cost of \$250/kW (current state of technology is 56%-75% efficiency and \$700/kW) [12,49]. These costs represent distributed hydrogen production and include compression, storage, and delivery. The electrolyzer has a capacity factor of 70% to adjust for seasonal and weekend/weekday fluctuations in demand and a 97% availability of the equipment.

Production of H<sub>2</sub> is an energy-consuming process, and may not be environmentally friendly [18,56]. In addition, the low density and extremely low boiling point of H<sub>2</sub> increase the energy costs of compression or liquefaction and the investment costs of storage and delivery. Distributed electrolysis case may play a role in the transition to the hydrogen economy when there is little delivery infrastructure for hydrogen [12]. Underground gas storage of hydrogen and oxygen in connection with the electrolysis may enable the electrolyzer to accommodate the variations in the power produced by renewable resources. The output-input efficiency cannot be much above 30%, while the advanced batteries have a cycle efficiency of above 80%. Even the most efficient fuel cells may not recover these losses [56,58-61].

## Methanol Production

Methanol synthesis needs carbon-rich feedstock (natural gas, coal or biomass), hydrogen, and a catalyst, mainly Cu/ZnO/Al<sub>2</sub>O<sub>3</sub> [26-34]. Methanol is produced almost exclusively by the ICI, the Lurgi, and the Mitsubishi processes. These processes differ mainly in their reactor designs and the way in which the produced heat is removed from the reactor. To improve their catalytic performance, the CuO/ZnO catalysts have been modified with various metals, such as chromium, zirconium, vanadium, cerium, titanium, and palladium [30-33,62]. The long-term stability of the catalysts may be improved by adding a small amount of silica to the catalysts at reaction conditions of 5 MPa, 523 K [63]. A high catalyst activity is related to a high copper surface area or small crystallite size combined with intimate contact with the zinc promoter. Table 6 shows some of the experimental reactor operating



Plant type	Capacity factor (%)	LCE	O&M with fuel	Transmission investment	Total LCE	Emission* mt CO <sub>2</sub> e/MWh
IGCC*	85	76.1	31.7	1.2	115.9	0.94-0.98
IGCC with CCS	85	97.8	38.6	1.2	147.4	0.94-0.98
NG-CC	87	15.7	45.5	1.2	64.4	0.55
NG-CC with CCS	87	30.3	55.6	1.2	91.3	0.55
Biomass	83	47.4	39.5	1.2	102.6	
Wind	35	64.1		3.2	80.3	
Wind-Offshore	37	175.4		5.8	204.1	
Solar PV	25	114.5		4.1	130.0	
Solar thermal	20	195.0		6.0	243.1	
Hydro	53	72.0	6.0	2.0	84.5	

\*Steam-electric generators in 2012 for calculating the amount of CO<sub>2</sub> produced per kWh<sup>2</sup>;  
IGCC: Integrated gasification combined cycle; O&M: Operations and Maintenance cost;  
CCS: Carbon capture and storage; NG: Natural gas; PV: Photovoltaic

**Table 1:** Estimated U.S. average levelized cost of electricity (LCE) 2012 \$/MWh for advanced generation resources entering service in 2019 [2].

Electrolyzer	Capacity (kW)	Efficiency % (HHV)	Efficiency % (LHV)
Alkaline	1-2,300	72	61
PEM	1-130	60	51
Solid Oxide	Pilot scale only	82	69

\*Norsk Hydro's 30,000 Nm<sup>3</sup>/hr (~ 150 MW) connected to a hydroelectric power plant, generating about 70,000 kg H<sub>2</sub>/day.  
The higher heating values for hydrogen: HHV= 39.42 kWh/kg and the lower heating value LHV= 33.31 kWh/kg.  
100% HHV efficiency translates into 84.5% efficiency based on LHV.

**Table 2:** Electrolyzer types\* [9-11].

Wind turbine capital cost (\$/kW)	1654	2067	2481
Electrolyzer energy use (kWh/kg H <sub>2</sub> )	47.5	50	60
Electrolyzer capital cost (\$/kW)	326	408	489
Wind farm availability (%)	90	88	86
Electrolyzer capacity factor (%)	99.5	98	96

**Table 3:** Sensitivity analysis changing the unit cost of H<sub>2</sub> with the production efficiency and electricity cost [9,10,55-57].

Water		Hydrogen		Oxygen		Water	
kg/hr	kmole/hr	kg/hr	kmole/hr	kg/hr	kmole/hr	kg/hr	kmole/hr
485	26.9	43.59	21.6	346.51	10.8	94.82	5.3

**Table 4:** Stream table of the norsk hydro atmospheric type electrolyzer unit [9,10].

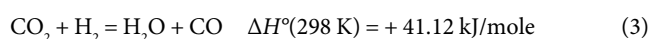
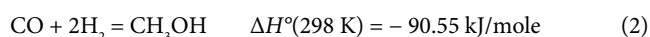
System energy required (includes compression)		Hydrogen production		Electrolyzer energy required	System power required
kWh/(Nm <sup>3</sup> )	kWh/kg H <sub>2</sub>	kg/h	kmole/hr	kWh/(Nm <sup>3</sup> )	kW
4.8	53.5	43.59	21.6	4.3	2330

**Table 5:** Energy usage for the Norsk electrolyzer [9,10].

Reactions	T, °C	P, bar
Based on all three reactions (1-3) [63]	250	50
Based on all three reactions (1-3) [65]	200-244	15-50
Based on reaction (1) and (2) [66]	215-270	50
Based on reaction (1) and (3) [67]	187-277	30-90
Based on reaction (1) and (3) [68]	180-280	51
Based on reaction (1) and (3) [69]	220-300	50-100

**Table 6:** Experimental conditions of methanol synthesis with the catalyst Cu/ZnO/Al<sub>2</sub>O<sub>3</sub>

temperatures and pressures with the catalyst Cu/ZnO/Al<sub>2</sub>O<sub>3</sub>. During the synthesis these following reactions occur [63-69]



Only two of these reactions are linearly independent and two reaction rate equations can describe the kinetics of the all reactions.

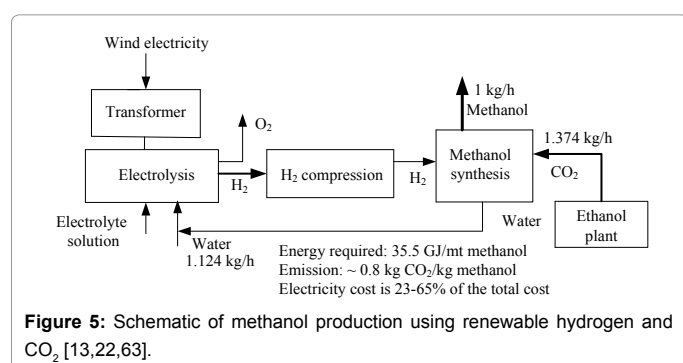
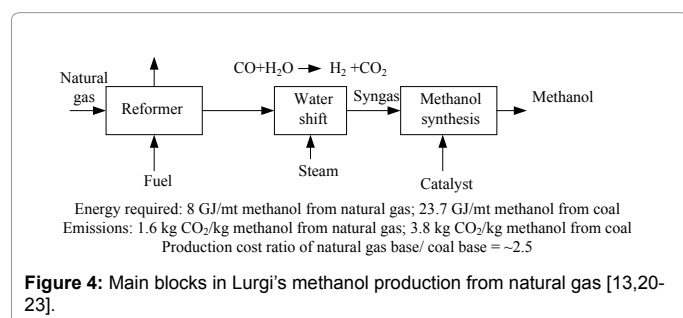
## Methanol from Natural Gas

Figure 4 shows the main blocks of natural gas-based methanol production. Three fundamental steps are: (i) natural gas reforming to produce syngas with an optimal ratio of [(H<sub>2</sub> CO<sub>2</sub>)/(CO + CO<sub>2</sub>)] = 2, (ii) conversion of syngas into crude methanol, and (iii) distillation of crude methanol. Methanol synthesis from natural gas has a typical energy efficiency of 75% and emits around 1.6 kg CO<sub>2</sub>/kg methanol [13]. Specific energy consumption for natural gas-based methanol is around 8.0 GJ/mt methanol [22]. Captured CO<sub>2</sub> is commonly reused internally in ammonia and some methanol plants.

Table 7 compares the cost of methanol production and emissions from fossil fuel resources. Coal-based syngas process has the highest emission of GHGs, which is around 2.8-3.8 kg CO<sub>2</sub>/kg methanol. The typical energy efficiency for the coal-based methanol is in the range of 48% to 61% [13,22]. Technical and economic analyses of methanol production from biomass-based syngas show that overall energy efficiency is around 55% based on HHV. The level of emission is around 0.2 kg CO<sub>2</sub>/kg methanol, which is mainly from biomass growing, harvesting, and transportation. Methanol from biomass or flue gas CO<sub>2</sub> is at least 2-3 times more expensive than the fossil-fuel based methanol [13,64-70].

## Methanol from CO<sub>2</sub> and H<sub>2</sub>

Converting CO<sub>2</sub> into chemicals is thermodynamically challenging, and inherently carries costs for the energy and hydrogen supply [22]. The conversions of reactions (1) to (3) with catalyst of Cu/ZnO/Al<sub>2</sub>O<sub>3</sub> are limited by the chemical equilibrium of the system. The temperature rise must be minimized in order to operate at good equilibrium values. However selectivity for methanol is high with a value of 99.7% at 5 MPa and 523 K with a H<sub>2</sub>/CO<sub>2</sub> ratio of 2.82 [63]. The energy efficiency for the concentrated CO<sub>2</sub> and hydrogen based methanol is around 46%. Figure 5 shows a schematic of renewable hydrogen production.



Process	Production cost \$/mt methanol <sup>1</sup>	Emissions kg CO <sub>2</sub> /kg methanol	Energy efficiency %
Natural gas based syngas	170	0.5-1.6	75
Coal based syngas	432	2.8-3.8	48-61
Biomass based syngas	723	0.2	51
CO <sub>2</sub> from flue gas	973	0.8	46

<sup>1</sup>The cost data<sup>13</sup> for 2005 has been updated using: Cost<sub>new</sub> = Cost<sub>old</sub> [CEPCI(2014)/CEPCI(2005)]  
CEPCI (2014) = 576.1 and CEPCI (2005) = 468 [70].

<sup>13</sup>This emissions account for methanol production process and the emissions occurring with the utilization of methanol.

**Table 7:** Methanol costs and emissions<sup>13</sup> [13,22,71].

Methanol synthesis from water, renewable electricity, and carbon may lead to renewable energy storage, carbon recycle, fixation of carbon in chemical feedstock, as well as extended market potential for electrolysis. For methanol production with coal as carbon source, 23.7 GJ/mt methanol and with CO<sub>2</sub> as carbon source 35.5 GJ/mt methanol are required.

Currently the cost for hydrogen from electrolysis is roughly twice of that from natural gas steam reforming. Therefore, methanol production from renewable hydrogen would increase the energy consumption; however, a significant GHG reduction may be possible [22]. Clausen et al. [70] used electrolytic H<sub>2</sub> in methanol production using the post combustion captured CO<sub>2</sub>. The alkaline electrolyzer is operated at 90°C and atmospheric pressure with an electricity consumption of 4.3 kWh/Nm<sup>3</sup> H<sub>2</sub> corresponding to an efficiency of 70% (LHV). With underground storage for hydrogen and oxygen and the electricity price during the off-pick hours of operation, the costs are estimated as \$15.0/GJ, \$20.0/mt CO<sub>2</sub>, and \$217/mt methanol (2010 \$), respectively. The electricity cost is around 23%-65% of the methanol production cost because of high stoichiometric hydrogen demand in the synthesis [66-68].

## CO<sub>2</sub> Capture and Compression

Some of the available sources for CO<sub>2</sub> are fermentation processes such as ethanol production plants, fossil fuel-based power stations, ammonia, and cement plants. Table 8 shows the equipment and operating costs to capture and liquefy 68 mt CO<sub>2</sub>/day and 272 mt CO<sub>2</sub>/day (the maximum capture rate for a typical 40 million gal/year ethanol plant). The estimated costs are for food grade CO<sub>2</sub> (99.98% minimum and <0.4 ppmv of sulfur) and also for less purified CO<sub>2</sub> suitable for enhanced oil recovery or sequestration [25].

## Methanol Production Plant

We have designed and simulated a methanol plant using renewable electrolytic H<sub>2</sub> and CO<sub>2</sub> supplied from an ethanol plant. The RK-SOAVE equation of state is used. The plant uses 19.1 mt H<sub>2</sub>/day and 138.4 mt CO<sub>2</sub>/day, and produces 99.9 mt methanol/day at 99.7-wt% together with 57.3 mt/day 98.3-wt% of waste water. Table S1 in the 'Supporting Information' presents the stream table representing the energy and material balances of the plant.

Figure 6 presents the process flow diagram for the methanol plant using CO<sub>2</sub> and H<sub>2</sub>. The feedstock is at the conditions associated with typical storage, with H<sub>2</sub> at 25°C and 33 bar and CO<sub>2</sub> at -25.6°C and 16.422 bar (liquid phase) [7,8,25]. The ratio of H<sub>2</sub> to CO<sub>2</sub> is held at of 3:1 to promote methanol synthesis. In the feed preparation block, the renewable H<sub>2</sub> and CO<sub>2</sub> are compressed to 50 bar in a multi-stage compressor and pump, respectively, and mixed with the recycle stream S9 in mixer M101. Stream S4 is the feed of the plug-flow reactor R101 where the methanol synthesis takes place. This multi-tube reactor has 15 tubes with a diameter 0.127 m and a length of 5 m, loaded with a total of 250 kg of catalyst. The reactor operates at 50 bar with a constant temperature of 235°C representing the Lurgi's low pressure isothermal system [66].

Langmuir-Hinshelwood Hougen-Watson (LHHW) kinetics formulations, with fugacities, are used for reactions (1) and (2). LHHW kinetics considers the adsorption of the reactants to the catalytic surface, the surface reactions to synthesize the methanol, and the desorption of the products from the catalytic surface [47,66]. The reactor output stream S5 is expanded in a turbine in order to cool down the outlet and produce power. This turbine produces 0.69 MW of electrical energy which can be fed back into the process or sold for revenue. In flash drum F101, stream S6 is separated into liquid (S6) and gas streams (S7). Stream S7 is crude methanol, which is separated from the water in the distillation tower T101. The product methanol is the distillate, while the wastewater is the bottoms flow of T101. The streams of methanol and water are cooled by the heat exchangers of E101 and E102, respectively, and are stored. Gas stream S8 is sent to a flow splitter SF101, in which 90% of S8 is recycled to the reactor after it is compressed in the multi stage compressor REC-COMP. Stream S9 is chosen as a tear stream. The mole fraction of methanol in the distillate is controlled by varying the reflux ratio and the ratio of bottoms flow to feed flow rate by using two design specifications in the Radfrac column T101. The column has 20 stages with a feed stage 17 and partial condenser. Methanol production has the potential for the best possible technology deployment ranging from 16% to 35% [65]. Therefore the design reflects that potential in a simple design delivering almost pure methanol and waste water containing less than 1% methanol.

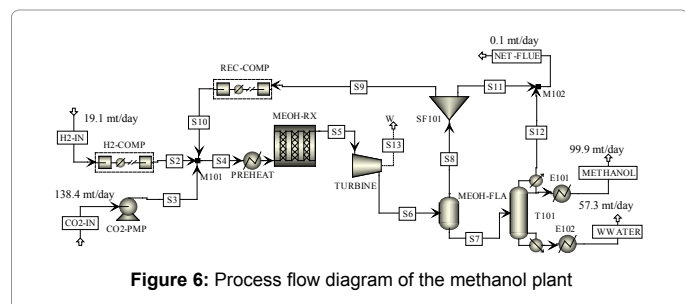
## Ammonia Production

Ammonia is synthesized by the catalytic reaction of H<sub>2</sub> and nitrogen gas at around 400-600°C and 200-400 atmospheres (Haber

Cost	68 mt CO <sub>2</sub> /day beverage grade	272 mt CO <sub>2</sub> /day beverage grade	272 mt CO <sub>2</sub> /day Non-beverage grade
Capital cost, \$	2,530,000	5,770,000	4,700,000
Capital cost, \$/mt CO <sub>2</sub>	37205	21213	17279
Electricity, \$/mt CO <sub>2</sub>	19.46	18.8	18.9

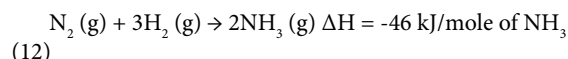
Electricity cost: \$0.10/kWh

**Table 8:** Estimated cost of CO<sub>2</sub> recovery options from ethanol plant (\$ 2006) [25]



**Figure 6:** Process flow diagram of the methanol plant

and Bosch process).



The sources of H<sub>2</sub> are steam reforming and/or water-gas shift from natural gas or gasification of coal, while an Air Separation Unit (ASU) supplies the nitrogen [71-73]. Figure 7 shows the both processes of renewable H<sub>2</sub> based and syngas-based NH<sub>3</sub> production.

## Air Separation Unit

ASU can produce nitrogen (99.999% purity) and oxygen (98% purity) for synthesis of ammonia using the air [72,73]. Ambient air is compressed in multiple stages (accounting for 86% of the total energy consumption) with inter-stage cooling to 6.45 bar and sent into the molecular sieve to remove residual water vapor, carbon dioxide, and atmospheric contaminants. Table 9 shows typical power consumptions. A larger plant with efficiency improvements (energy consumption of less than 10%) and process optimization would deliver air liquefaction at around 0.4 MWh/mt liquid nitrogen. Operation and Maintenance (O&M) costs typically amount to between 1.5% and 3% of the plant purchase price per annum. Production cost is around \$54/mt nitrogen for a 300 mt/day and \$49/mt nitrogen for a 600 mt/day capacity [71-73].

## Ammonia Production Plant

Figure 8 shows the process flow diagram for the ammonia plant. Production of ammonia is based on the Haber-Bosch synthesis process with a high pressure reactor in the presence of porous iron oxide. Typically for ammonia synthesis these conditions are about 150 atmospheres and 370-500°C. Under equilibrium conditions the proportion of reactants and the product of a chemical reaction are balanced and determined by the existing physical conditions such as pressure, temperature and concentrations. Since the reaction is exothermic, lowering the temperature in the reactor will increase the yield of ammonia. However, this also slows down the reaction therefore, for higher efficiency; the temperature is kept as high as possible. Increasing the pressure will increase the yield of ammonia but there is a limit in pressure for safety reasons [41,42].

The nitrogen is supplied by an air separation unit SEP 101, to

produce 1202.66 mt/day anhydrous ammonia. The ammonia process is designed and simulated by using the RK-SOAVE equation of state property method. The ammonia plant uses 217.71 mt/day H<sub>2</sub> and 1009.15 mt/day nitrogen, and produces 1202.66 mt/day 99.9 wt % ammonia. The flow rate of ammonia is maximized to be 2943 kmol/hr and its composition to be 0.99wt% NH<sub>3</sub>, using the constrained optimization option. There is a slight loss of ammonia in the stream BLEED. Air is separated in SEP 101, and the feeds of nitrogen and hydrogen at 20.27 bar are mixed in M101. This mixture is compressed to about 212 bar in compressors C101 and C102. Temperature of this mixture is adjusted in heat exchanger E201. In reactor R201 the ammonia synthesis takes place at around 556°C and 212 bar with a platinum group metal such as ruthenium [40-42]. The reactor R201 is a RGIBBS reactor and estimates the equilibrium composition of the reactor by Gibbs free energy minimization. The output of the reactor is conditioned in heat exchangers E202 and E203 and sent to adiabatic flash drums FL301 and FL302, which operate at 203 and 12 bar, respectively. The bottom flow of FL302 is the product ammonia at -26°C and 12.4 bar. Stream table and overall mass and energy balances for the ammonia plant are presented in Table S3 and S4 within the "Supporting Information." There is a large energy difference between the input and output, and must be compensated by utilities from outside in the form of cooling water, steam, electricity, and refrigeration.

## Sustainability and Economic Analyses

### Sustainability analysis

The integral methanol production facility consists of three units: an electrolytic hydrogen production, CO<sub>2</sub> capture and storage, and the methanol production. Similarly, the integral ammonia production facility consists of three units: an electrolytic hydrogen production, ASU, and the ammonia production. Figures 9 and 10 show these integral facilities subject to sustainability and economic analyses. Table 10 shows the main results of the material and energy usages, as well as the CO<sub>2</sub> emissions for the integral facilities. The energy costs are estimated by the unit cost of utilities listed in Table 11.

The integral methanol facility requires 19.08 mt H<sub>2</sub>/day and 138.38 mt CO<sub>2</sub>/day in total. The total emissions of CO<sub>2</sub> from each unit are -111.54 mt CO<sub>2</sub>/day, 18.51 mt CO<sub>2</sub>/day, and 8.77 mt CO<sub>2</sub>/day for the methanol production, H<sub>2</sub> production, and CO<sub>2</sub> capture and storage, respectively. The net carbon fee is -\$9.3/h for the methanol facility and \$69.89/h for the ammonia facility based on a set value of \$2/mt CO<sub>2</sub>e. As Table 10 shows, the values of net duty and cost are the highest for the hydrogen production units used in methanol and ammonia productions.

The integral ammonia facility requires 217.72 mt H<sub>2</sub>/day and 1009.15 mt N<sub>2</sub>/day in total. The total emissions of CO<sub>2</sub> from each unit are 838.78 mt CO<sub>2</sub>/day, 211.18 mt CO<sub>2</sub>/day, and 111.47 mt CO<sub>2</sub>/day for the ammonia production, H<sub>2</sub> production, and ASU, respectively.

Figure 11 presents an approximate energy balance with the energy required for the electrolyzer, carbon capture and storage, and total duty required in methanol production versus energy content in methanol as fuel combusted fully. The energy efficiency for the integral facility is around 58%.

Figure 12 shows an approximate energy balance with the energy required for the electrolyzer, nitrogen production through the ASU, and the total duty required for the ammonia production versus the energy content in ammonia as a fuel combusted fully. The total energy efficiency for the integral facility is around 35%.

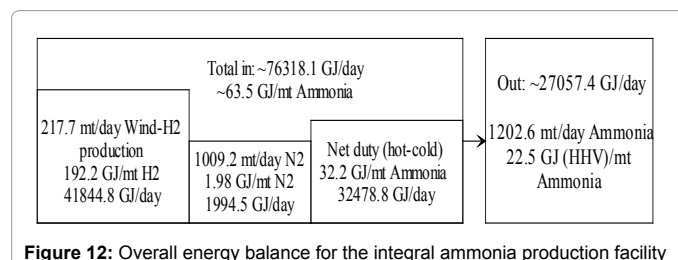
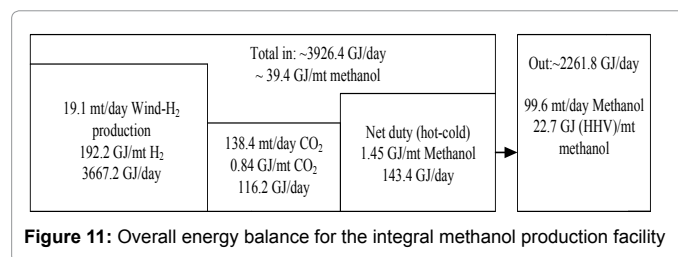
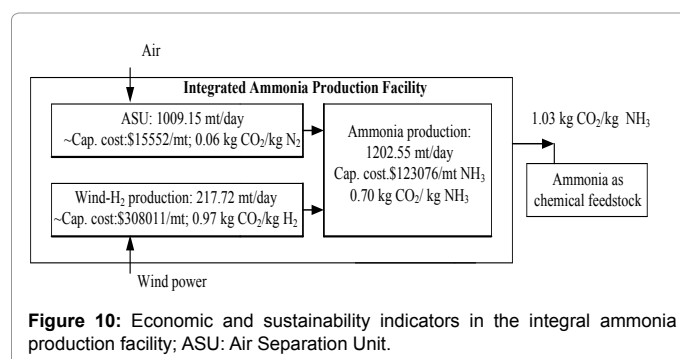
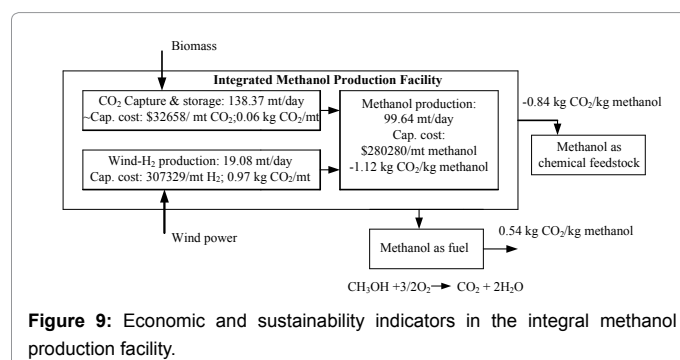
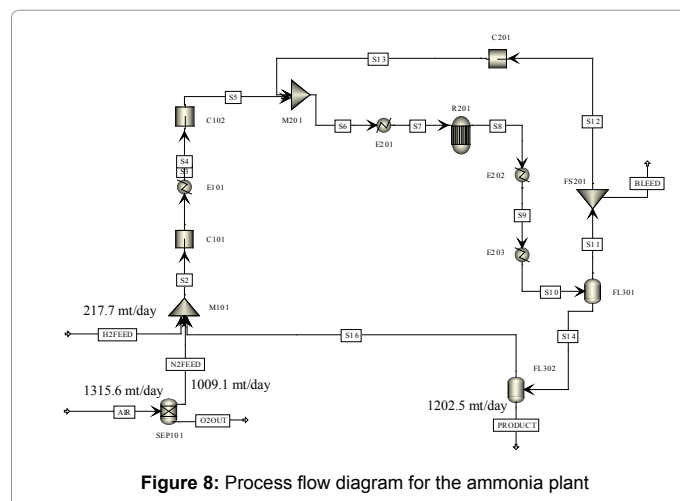
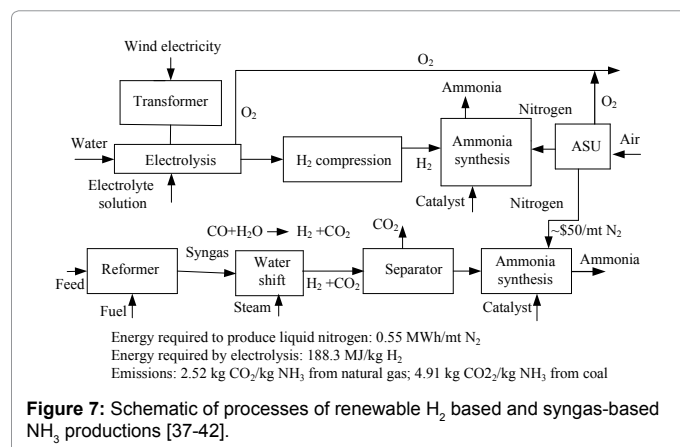


Table 12 presents the following sustainability metrics that are estimated for the integral methanol and ammonia facilities:

- Material intensity (nonrenewable energy/unit mass of product)
- Energy intensity (nonrenewable energy/unit mass of product)
- Potential environmental impact (pollutants and emissions/unit mass of product)

The overall facility emissions of CO<sub>2</sub> are normalized with respect to methanol and ammonia capacities. The material intensity metrics show that the methanol facility requires 1.39 mt CO<sub>2</sub>/mt methanol. The environmental impact metrics shows that the integral methanol facility reduces -0.84 kg CO<sub>2</sub>/kg methanol when utilizing it as a chemical feedstock, and recycles 0.53 kg CO<sub>2</sub>/kg methanol after its complete combustion, as seen in Figure 9. On the other hand, the environmental impact metrics for the integral ammonia facility is 1.03 kg CO<sub>2</sub>/kg ammonia, as seen in Figure 10. The duty (heating-cooling) becomes negative due to excessive cooling required in the ammonia facility.

## Economic analysis

The economics analyses of the integral methanol and ammonia plants are based on the Discounted Cash Flow Diagrams (DCFD) prepared for a ten-year of operation using the current economic data. Based on the equipment list from the process flow diagrams (Figures 6 and 8), bare module costs are estimated and used as Fixed Capital Investments (FCI). Chemical Engineering Plant Cost Index [48] (CEPCI-2014) (=576.1) is used to estimate and update the costs and capacity to the present date by

$$\text{Cost}_{\text{New}} = \text{Cost}_{\text{New}} \frac{\text{CEPCI}_{\text{New}}}{\text{CEPCI}_{\text{Old}}} \left( \frac{\text{Capacity}_{\text{New}}}{\text{Capacity}_{\text{Old}}} \right)^x \quad (5)$$

Where  $x$  is the factor, which is usually assumed to be 0.6. Working capital is 20% of the FCI. Depreciation method is the Maximum Accelerated Cost Recovery System (MACRS) with a 7-year recovery period [74]. After estimating the revenue and the cost of production, DCFDs are prepared. The details can be found within the 'Supporting Information.' DCFDs generate the three economic feasibility criteria that are Net Present Value (NPV), Payback Period (PBP), and Rate of Return (ROR). At least two out of three criteria should be favorable for



the operation to be feasible. These criteria are favorable if NPV  $\geq 0$ , PBP  $\leq$  useful operational years; and ROR  $\geq i$ , where  $i$  is the internal interest rate. In addition, the economic constraint (EC) and the unit product cost (PC) are also estimated

$$EC = \frac{\text{Average Discounted Annual Cost of Production}}{\text{Average Discounted Annual Revenue}} \quad (6)$$

$$PC = \frac{\text{Average Discounted Annual Cost of Production}}{\text{Capacity of the plant}} \quad (7)$$

The PC takes into account the Operating and Maintenance (O&M) costs. An operation with  $EC < 1$  shows the opportunity to accommodate other costs and improve the cash flows of the operation toward a positive NPV.

The estimated approximate values of the FCIs are \$5.87 million for the wind-based electrolytic  $H_2$  production unit, \$4.52 million for the  $CO_2$  production unit, and \$28 million for the methanol production unit. The  $H_2$  production includes the compression, storage, and dispensing from a centralized production facility with an average electricity cost of 0.045/kWh. Therefore, the total value of the FCI is around \$38.39 million.

The distribution of unit capital costs for the integral methanol production facility shows that the contribution from wind-based  $H_2$  is the highest (Figure 9). The cost of  $H_2$ , which makes the NPV = 0, is \$0.88/kg  $H_2$  when the selling price of methanol is \$600/mt with the corresponding values of  $EC = 0.85$  ( $< 1$ ) and  $PC = \$518/\text{mt}$  methanol ( $< \$600/\text{mt}$ ). Global prices of methanol vary widely; the prices in 2014 are \$435/mt in Europe, \$482/mt in North America, \$410/mt and in Asia Pacific [75]. Compared with natural gas-based methanol, the cost of renewable methanol production is almost five times higher. Only the biomass production cost is comparable, as seen in Table 13. The cost of renewable hydrogen and the selling price of methanol affect the economics of the renewable methanol.

The approximate value of FCI for the ammonia process is around \$148.5 million, while the values of FCIs for the ASU and wind-based electrolytic  $H_2$  production unit are around \$15.6 million and \$66.9 million, respectively. The capital cost of the integrated production, including the ammonia process, the ASU, and the  $H_2$  production unit, becomes \$231.0 million. An average selling price of ammonia is around \$700.0/mt (2014 \$) [76]. The cost of  $H_2$ , which makes the NPV = 0, is \$2.33/kg  $H_2$  when the selling price of ammonia is \$700/mt with the corresponding values of  $EC = 0.95$  ( $< 1$ ) and  $PC = \$662.9/\text{mt}$  methanol ( $< \$700/\text{mt}$ ). The details of the economic analysis of the ammonia plant are given in the 'Supporting Information.'

## Assessment of Renewable Methanol and Ammonia Productions

Minimum and maximum current world-wide productions of methanol are around 55 to 5000 mt/day. Methanol has half of the volumetric energy density relative to gasoline or diesel; however, it can be used in the direct methanol fuel cell [13-15,20,21,29,34,36]. Renewable hydrogen-based methanol would recycle carbon dioxide as a possible alternative fuel to diminishing oil and gas resources [77-79]. It is also used as a chemical feedstock to ultimately fix the carbon. This would lead to a "methanol economy" [18,19]. There are already vehicles which can run with M85, a fuel mixture of 85% methanol and 15% gasoline [1,18-22]. Methanol can be used with the existing distribution infrastructure of conventional liquid transportation fuels. In addition, fuel cell-powered vehicles are also in a fast developing stage, although

they are not yet available commercially [1,2,19].

Table 13 shows the specific energy consumptions and emissions in producing methanol and ammonia by various feed stocks [22]. The coal-based process has the emissions of 3.8 kg  $CO_2$ /kg methanol, while natural gas-based process leads to 1.6 kg  $CO_2$ /kg methanol. Lifecycle  $CO_2$  emission is around 0.8 kg  $CO_2$ /kg methanol for the flue gas based methanol. Around 50% of these emissions are due to the  $CO_2$  capture processes [22,80].

Current capacities for ammonia vary from 1,000 to 2,000 mt/day or 360,000 to 720,000 mt/year.  $NH_3$  can be used as fertilizers, industrial chemicals, and fuel. Ammonia cracking is endothermic and depends on the catalyst [37,38]. Ammonia has a capacity of 17.6 wt% for  $H_2$  storage; however, considerable energy is required to release  $H_2$  from ammonia. Ammonia synthesis coupled with hydrogen production may increase efficiency. Ammonia can burn directly in an internal combustion engine and can be converted to electricity directly in an alkaline fuel cell, or converted to  $H_2$  for non-alkaline fuel cell. However, Polymer Electrolyte Membrane (PEM) fuel cell technology is incompatible in the presence of ammonia ( $>0.1$  ppm) [37]. For sites in a remote island, ammonia fuel may become competitive around \$10/gallon of diesel fuel [39-41].

When it is produced from natural gas, ammonia production cost depends on the price of natural gas; for example, for \$4.5/MMBtu natural gas,  $NH_3$  production cost is around \$180/mt, while for \$7.0/MMBtu natural gas,  $NH_3$  production cost becomes \$260/mt at 2006 \$. Only 60-65% of the energy input of natural gas to the process is contained in the product ammonia. Replacing natural gas with coal as the feedstock increases energy consumption and production costs 1.7 times and the investment cost 2.4 times [37-39,73]. The cost of ammonia from renewable hydrogen ranges between \$660/mt and 1,320 \$/mt, which is higher than both coal and natural gas based-ammonia production costs [22].

Emission for a natural gas-based ammonia is around 2.52 mt  $CO_2$ /mt  $NH_3$ , while coal-based ammonia produces nearly 4.91 mt  $CO_2$ /mt  $NH_3$ . The emission of  $CO_2$  based on natural gas represents a lower limit for the GHG emissions from ammonia production. Some of the  $CO_2$  emitted is captured and subsequently used for the production of urea [22,37,38,77]. Energy consumption, as well as the capital cost, in ammonia production is higher than of that for methanol production [22]. The best possible technique for  $NH_3$  production uses  $H_2$  from renewable energy sources. Hydrogen production is one of the largest energy-consuming steps in the production of ammonia and methanol. Capital cost for a centralized 20000 mt  $H_2$ /year plant is around \$60 million (2011\$) with operational cost estimated at \$3.3 million/year. The investment costs of a centralized water electrolysis plant would be roughly one third of the investment costs of a conventional natural gas based plant of equivalent production capacity [22]. As Table 13 shows, this is by far the highest energy consuming process step in the overall scheme and dominates all subsequent steps, such as hydrogen compression and, in the case of ammonia production, the air separation unit for production of nitrogen from air [22].

Process Steps	kWh/Nm <sup>3</sup>	MJ/Nm <sup>3</sup>	MJ/kg	kg $H_2$ /Nm <sup>3</sup>	kg $N_2$ /Nm <sup>3</sup>	\$/mt $N_2$
Electrolysis	4.7	17.0	188.3	0.09		
ASU	1.0	4.0	3.1		1.17	49(600 mt $N_2$ /day)

**Table 9:** Specific energy consumptions for hydrogen and nitrogen [22,71-73]

Material metrics	Integral methanol production			Integral ammonia production		
	Methanol production	H <sub>2</sub> prod.	CO <sub>2</sub> C&S	NH <sub>3</sub> prod.	H <sub>2</sub> prod.	ASU
CO <sub>2</sub> Input, mt/day	138.37					
H <sub>2</sub> Input, mt/day	19.08			217.72		
N <sub>2</sub> Input, mt/day				1009.2		
Methanol production, mt/day	99.66					
Ammonia production, mt/day				1202.6		
<b>Energy intensity metrics</b>						
Total heating duty, MW	4.60	42.49	1.05	103.54	484.89	23.08
Total cooling duty, MW	2.93	0.12	0.03	162.32	1.40	0
Net duty (heating - cooling), MW	1.67	42.37	1.02	-58.78	483.49	23.08
Total heating cost flow, \$/h	59.18	3292.83	81.31	2648.9	37579	1789
Total cooling cost flow, \$/h	2.24	0.09	0.02	1236	4.85	
Net cost (heating + cooling), \$/h	61.42	3292.92	81.33	3885	37584.08	1789.04
<b>Environmental impact metrics</b>						
Net stream CO <sub>2</sub> e, mt/day	-138.37	0	0	0	0	0
Utility CO <sub>2</sub> e, mt/day	26.83	18.51	8.77	838.78	211.18	111.47
Total CO <sub>2</sub> e, mt/day	-111.53	18.51	8.77	838.78	211.18	111.47
Net carbon fee, \$/h	-9.29	1.54	0.73	69.89	17.60	9.29

<sup>a</sup>US-EPA-Rule-E9-5711; natural gas; carbon fee: \$2/mt.

**Table 10:** Sustainability indicators for the methanol and ammonia plants<sup>a</sup>

Utilities	Energy price, \$/MJ	T <sub>in</sub> °C	T <sub>out</sub> °C	Factor <sup>a</sup>	U <sup>b</sup> kW/m <sup>2</sup> K
Electricity	\$0.0775/kW h			0.58	
Cooling Water	\$0.09/mt	20	25	1	3.75
Medium Pressure Steam	2.2 × 10 <sup>-3</sup>	175	174	0.85	6.00
High Pressure Steam	2.5 × 10 <sup>-3</sup>	250	249	0.85	6.00
Refrigeration	3.3 × 10 <sup>-3</sup>	-39	-40	-1	1.30

<sup>a</sup>CO<sub>2</sub> energy source efficiency factor; <sup>b</sup> Utility side film coefficient for energy analysis.

**Table 11:** Unit energy cost for various utilities with energy source of natural gas for 2014 [47].

Metrics	Integral methanol plant	Integral ammonia plant
<b>Material metrics</b>		
CO <sub>2</sub> used/Unit product	1.39	
N <sub>2</sub> used/Unit product		0.84
H <sub>2</sub> used/Unit product	0.19	0.18
<b>Energy intensity metrics</b>		
Net duty/unit product, MWh/mt	9.55	-1.17
Net cost/Unit product, \$/mt	828.67	863.33
<b>Environmental impact metrics</b>		
Total CO <sub>2</sub> e/Unit product	-0.85	1.03
Net carbon fee/Unit product, \$/mt	-1.70	2.07

**Table 12:** Sustainability metrics for the integral methanol and ammonia plants

Process	kg H <sub>2</sub> /kg prod.	H <sub>2</sub> prod./comp.	Average prod.	BPT	Theor min.	Average kg CO <sub>2</sub> /kg prod.
Methanol from CO <sub>2</sub>	0.189	37.06				
Syngas-coal methanol	0.126	24.20	24.0	20.1	5.1	2.83
Syngas-NG methanol			13.9	9.0-10	5.1	0.52
Ammonia	0.178	35.57				
syngas-NG Ammonia			15.4	7.2-9.0	5.8	2.52
Syngas-coal Ammonia			27.9	22.0	8.1	4.91

SEC: Specific energy consumption that includes fuel, steam and electricity for the process.

BPT: Best possible technology; GHG: greenhouse gas emissions as CO<sub>2</sub> equivalent per ton of product;

CO<sub>2</sub>e includes CO<sub>2</sub>, CH<sub>4</sub>, and NO<sub>x</sub>.

**Table 13:** Specific energy consumptions and emissions for ammonia and methanol productions [22]

Economics and sustainability indicators	Weighting factor:0-1	Fossil-methanol	Non-fossil-methanol	Fossil-ammonia	Non-fossil-ammonia
<b>Economic indicators</b>					
Net present value NPV	1	+	-	+	-
Payback period PBP	0.8	+	-	+	-
Rate of return ROR	0.8	+	-	+	-
Economic constraint EC	0.9	+	-	+	-
Impact on employment	1	+	+	+	+
Impact on customers	1	+	+	+	+
Impact on economy	1	+	+	+	+
Impact on utility	0.7	-	+	-	+
<b>Sustainability indicators</b>					
Material intensity	0.7	-	+	-	+
Energy intensity	0.8	+	-	+	-
Environmental impact GHG in production	0.8	-	+	-	+
Environmental impact GHG in utilization	0.8	-	-	+	+
Toxic/waste material emissions Process safety and Public safety	1	-	+	-	-
Potential for technological improvements and cost reduction	0.8	-	+	-	+
Security/reliability	0.9	-	+	-	+
Political stability and legitimacy	0.8	-	+	-	+
Quality of life	0.8	-	+	-	+
Total positive score		8	11	9	11
Total minus score		9	-6	-8	-6
Net score (positive-minus)		-1	+5	+1	+5
<b>Weighted total score</b>		<b>+0.2</b>	<b>+5.4</b>	<b>+2</b>	<b>+4</b>

**Table 14:** Multi-criteria decision matrix for feasibility evaluation of chemical processes and energy systems

Tallaksen and Reese [38] compared the renewable and with fossil-based ammonia productions in terms of energy use and carbon emissions using the Life Cycle Assessment (LCA) methods. Renewable ammonia production requires around 60 GJ of electricity/mt ammonia. This is considerably more total energy than conventional fossil fuel based produced ammonia, however it requires less fossil energy and results in less GHG emissions. The boundary of LCA for the wind to ammonia contains wind power, water electrolysis, hydrogen compression, nitrogen separation and compression, ammonia production and ammonia storage. LCA is more focused on environmental issues rather than raw material depletion [38].

Main chemical storage of electricity involves the production of hydrogen, synthetic natural gas, and chemicals, which are mainly methanol and ammonia. Combination of several storage applications together may help electricity storage to be more feasible. The initial investment requires a cost per unit of power (\$/kW) and a cost per unit of energy capacity (\$/kWh), which are technology dependent [77]. The economics of electricity storage are influenced by the type of storage technology, electricity price, the frequency of charging and discharging cycles, and the system in which the storage facility is located. Besides, one needs to consider direct and localized impacts of the technology and the generation source used [77].

### Assessment of Chemical Processes by a Multi-Criteria Decision Matrix

Beside the economics analysis, sustainability metrics should also be used to evaluate the feasibility of chemical processes [81-84]. Table 14 shows a Pugh decision matrix [85] developed using '+' and '-' for the ratings to assess the methanol and ammonia production plants. Four scores generated show the number of plus scores, minus scores, the overall total, and the weighted total. The weighted total adds up the

scores times their respective weighting factors. The totals are guidance only for decision making. If the two top scores are very close or very similar, then they should be examined more closely to make a more informed decision. Renewable energy-based systems may require the combined use of scenario building and participatory multi-criteria analysis for sustainability assessment [84].

Table 14 indicates the weighted decision matrix to compare the plants producing methanol and ammonia from fossil and non-fossil resources. The weight factor can be adjusted with respect the location, energy policies, and energy costs and security. With the weight factors and the combined economic and sustainability indicators, the decision matrix has estimated the highest weighted scores for the renewable methanol and ammonia production facilities. The positive weighted score for the renewable methanol (+5.4) is slightly better than the renewable ammonia production (+4). These scores indicate the overall impact of sustainability indicators beside the economics.

### Conclusion

Renewable hydrogen, methanol, and ammonia productions may lead to renewable electricity storage and reduce the carbon emissions either by recycling and/or fixation of the carbon. The cost of hydrogen production plays an important role within the economics of the renewable methanol and ammonia productions and determines the scope of improvements necessary for feasible operations. The economic analysis shows that the cost of electrolytic hydrogen is critical in the economics of renewable methanol and ammonia plants at the capacities assumed in this study and using the currently available technologies. Despite its poor overall efficiency and high up-front capital costs, chemical storage may provide the large-scale and long-term storage requirements of a mixed renewable power generation. Multi-criteria decision matrix, containing the sustainability indicators,

show that chemical processes that use non-fossil fuels may achieve better overall weighted scores. This helps accounting the cost of environmental damage from using fossil fuels in the overall assessment of feasibility for chemical process and energy systems. This is in line with the need for the development of low-carbon chemical processes and energy technologies in order to address the global challenges of energy security, climate change, and economic growth.

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